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# **RESEARCH ARTICLE**

# THERMODYNAMIC CONTRIBUTION TO THE SOLUBILITY EQUATION

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## ARTICLE INFO ABSTRACT

#### Article History:

Received 5<sup>th</sup>, March, 2015 Received in revised form 12<sup>th</sup>, March, 2015 Accepted 6<sup>th</sup>, April, 2015 Published online 28<sup>th</sup>, April, 2015 An attempt to formulate the solubility equation was studied using thermodynamic data of both solute and solvent. The given equations predict quantitatively the solubility of different solutes in different solvents. Also, Miscibility and immiscibility of different solvents are estimated. The provided equations may be extended to be a general equations of solubility.

#### Key words:

Solubility, thermodynamic data, energy interaction, energy – mass distribution.

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## INTRODUCTION

The task of solubility has been treated by various text books and articles. Solubility parameters have been introduced, Hildbrand solubility parameter and Hansen solubility parameters. Hildbrand solubility parameter is the total van der Waals force, however, which is reflected in the simplest solubility value. The solubility parameter is a numerical value that indicates the relative solvency behavior of a specific solvent. It is derived from the cohesive energy density of the solvent, which in turn is derived from the heat of vaporization. The Hildebrand solubility parameter for a pure liquid substance is defined as the square root of the cohesive energy density.

$$C = [(Hv-RT)/V_m]^{1/2}$$

where Hv is the heat of vaporization, and  $V_m$  the molar volume. (RT) is the ideal gas (PV) term, and it is subtracted from the heat of vaporization to obtain an energy of vaporization <sup>(1)</sup>. Hansen Parameters is the most widely accepted three component system to date which divide the total Hildebrand value into three parts: a dispersion force component, a hydrogen bonding component, end a polar component.

Where

2= t	Total Hildebrand parameter
2= d	dispersion component
2= p	polar component
2 = h	hydrogen bonding component

Thermodynamics requires that the free energy of mixing must be zero or negative for the solution process to occur spontaneously. The free energy change for the solution process is given by the relation:

$$G^M = H^M - TS^M$$

where

 $G^{M}$  is the free energy of mixing,

 $H^M$  is the heat of mixing, T is the absolute temperature,

and

 $TS^{M}$  is the entropy change in the mixing process.

The Gibbs energy can be written in terms of chemical potentials of components A and B:

 $G(\min) = xA \quad \mu(A,T) + xB \quad \mu(B,T)$ 

The thermodynamic activity is defined as:  $(A) = (A)^2$ 

 $RT \ln aA = \mu (A) \text{ and } RT \ln aB = \mu (B)^{2,3}$ 

An equation was reported to estimate the quantity of solute that saturates a solvent:

$$\ln x = \frac{\Delta H_{fus}}{R} \left( \frac{1}{T} - \frac{1}{T_M} \right)$$

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Where

x : mole fraction of solute

H<sub>fus</sub>: enthalpy of fusion of solute

T: absolute temperature

T<sub>M</sub>: melting temperature

However, the detailed content of this equation should not be treated too seriously because it is based on highly questionable approximations, such as the ideality of the solution. One aspect of its approximate character is that it fails to predict that solutes will have different solubilities in different solvents, for no solvent properties appear in the expression. 4, 5 The term of solute activity in a certain solvent was added to the last equation in order to correct the solubility quantifications. The solubility of various compounds were determined using the corrected equation and computational methods like conductorlike screening (COSMO)-based activity coefficient models and coefficient conductor-like screening segment activity (COSMO-SAC) 6,7

# **METHODOLOGY**

The solubility is considered as energy interaction between solute and solvent. The quantity of solute that will dissolves in a certain solvent is affected by different factors and the limit at which solubility stops. The factors affecting solubility are treated in this work as the breaking force which exhibit the capability of solvent to separate the molecules of solute, potential energies of both solute and solvent, and interpotential between solute molecules and solvent molecules. The limit at which solubility stops is related to the fusion energy of either solute or solvent which is lower. The limit of solubility does not mean the maximum quantity of solute that will dissolve but the maximum ratio of energy that limits the solubility, as will be illustrated bellow. The variables which will be used in this study are the energy of formation, the energy of vaporization, the energy of fusion and the lattice energy and the molar mass:

 $\mathbf{F} = \mathbf{H}_{\mathbf{f}} - \mathbf{RT}$ 

Where F is the energy of formation (considered as the potential energy)

H<sub>f</sub> is enthalpy of formation R is gas constant =  $8.31451 \text{ J} \cdot \text{K}^{-1} \cdot \text{mol}^{-1}$  $\mathbf{F}_{\mathbf{M}} = \mathbf{F}/\mathbf{M}$ Where  $\mathbf{F}_{\mathbf{M}}$  is the potential energy per unit mass M is the molar mass  $V = H_{vap} - RT$ V is the energy of vaporization (considered as the interpotential energy) H<sub>vap</sub> is the enthalpy of vaporization  $V_M = V/2M$ Where  $V_{M}$  is the interpotential energy per unit mass  $\mathbf{E}_{\mathbf{M}} = \mathbf{F}_{\mathbf{M}} + \mathbf{V}_{\mathbf{M}}$  $\mathbf{E}_{\mathbf{M}}$  is the total potential energy per unit mass  $J = H_{fus} - RT$ Where J is energy of fusion  $H_{\text{fus}}$  is the enthalpy of fusion Latt =  $H_{Latt} - RT$ Where

Latt. is the lattice energy

H<sub>Latt</sub> is the lattice enthalpy

T is the absolute temperature and set at 298 K

### A. Solubility of solid in liquid

The solubility of solid materials in liquid is divided into two parts, solubility of non ionic solids and solubility of ionic solids.

### A.1. Solubility of non ionic solids

The equation taking the general formula of

 $\mathbf{n} = \mathbf{S}_{\mathbf{G}} \cdot \mathbf{S}_{\mathbf{T}} \cdot \mathbf{S}_{\mathbf{c}} \qquad \mathbf{Eq.1}$ 

where

 $\mathbf{n}$  is the number of moles of solute the dissolves in one mole of solvent.

 $\mathbf{S}_{\mathbf{G}}$  is the gradient ratio of solubility

 $\boldsymbol{S}_{T}$  is the tunneling ratio of solubility

 $\mathbf{S}_{\mathbf{c}}$  is the correction factor

This formula has different factors as will be illustrated. The solubility equation of a solute in a certain solvent will be combined from this general form according to certain rules.

### Gradient ratio of solubility (S<sub>G</sub>)

The gradient term represents the ratio of solute that dissolves in solvent due to the difference in potential between solute and solvent.

 $S_G = S_{gf} \cdot S_{gr} \cdot S_{ge}$ 

 $S_{gf}$  is the breaking force

 $S_{gr}$  is the gradient factor of solubility (ratio of solute that allowed to dissolve due to interpotential difference)  $S_{ge}$  is the tunneling term between two limits of solubility

# The Breaking Force (S<sub>gf</sub>)

The potential energy of molecule is taking as its energy of formation as considered by the semi-empirical method of calculation  $^{8}$ . By simulation to the electric potential energy equation  $^{9}$ , we will obtain:

F = q/4 r

and by simulation to the electric force between two point charges  $^{\left(9\right)}$ 

(Force =  $q_1q_2/4$  r<sup>2</sup>) we can approximate the breaking force between two different molecules 1, 2:

 $S_{gf} = F_1 F_2 / F_2^2 = F_1 / F_2$ 

Where  $F_1$ ,  $F_2$  are the energy of formation of solvent and solute respectively.

 $\begin{array}{ll} S_{gf} \mbox{ is applied when } F_1 \!\!<\! F_2 & \mbox{Rule. 1} \\ F_{Latt.} = F_1 F_2 / (Latt.)^2 \\ F_{Latt.} \mbox{ is additional breaking force in case of solubility of ionic compounds} \end{array}$ 

### The gradient factor of solubility $(S_{gr})$

1

The ratio of solute that is allowed to dissolve is limited by the fusion energy of solute or solvent which is lower in value and is taken as J/V. The potential difference that allow solubility is taken as V/F. Here we will deal with five categories:

- 1.  $V_1/F_1 > V_2/F_2$
- 2.  $V_1/F_1$   $V_2/F_2$   $(V_1/F_1$  0.95  $V_2/F_2)$
- 3.  $V_1/F_1 < V_2/F_2$
- 4. Solubility of solute with  $E_{M2} < 1$  in solvent with  $E_{M1} > 1$
- 5. Solubility of solute with  $E_{M2} > 1$  in solvent with  $E_{M1} < 1$

The subscripts 1,2 refer the solvent and solute respectively. J/V tunneling factor (S<sub>ge</sub>)

The term tunneling is due to the similarity of this part of equation to the tunneling effect law in quantum mechanics.

$$S_{ge} = e^{-(\left|\frac{J2}{V2} - \frac{J1}{V1}\right|)^{1/2}}$$

It represents the tunneling between the two limit if solubility,  $J_1/V_1$  and  $J_2/V_2$ .

Now we will discuss the categories and incorporate the explanation of  $S_T$ ,  $S_c$  during it.

## Category. 1 : $V_1/F_1 > V_2/F_2$

#### This category is divided into three cases

- 1.  $V_1/F_1 V_2/F_2 > J/V$  ( J/V of solvent or solute which is lower)
- 2.  $V_1/F_1 V_2/F_2 = J/V$
- 3.  $V_1/F_1 V_2/F_2 < J/V$

## Case 1: $V_1/F_1 - V_2/F_2 > J/V$

The gradient factor is stated as follows:

$$\mathbf{S}_{G} = \frac{F_{1}}{F_{2}} \cdot \frac{J/V}{\frac{V_{2}}{F_{2}} - \frac{V_{1}}{F_{1}}} \cdot e^{-\left(\left|\frac{J_{2}}{V_{2}} - \frac{J_{1}}{V_{1}}\right|\right)^{1/2}}$$

The tunneling part  $(S_T)$ 

It represents the tunneling between different potentials of solute and solvent

2



#### Where

$V_{M2} < V_{M1}$	Rule. 2
$E_{M1} < 0.95. E_{M2}$	Rule. 3

## The correction factor S<sub>c</sub>

It is either decreasing factor  $S_{cd}$  or increasing factor  $S_{ci}$ depending on the relation between the total potential energy per unit mass of both solute and solvent.

#### **Decreasing factor** (S<sub>cd</sub>)

$$S_{cd1} = e^{-(\frac{E_{M1}}{2.E_{M2}})^{1/2}}$$

 $\begin{array}{ll} 4.E_{M2} & 0.95.F_{M1} \\ E_{M2} > 2. \ E_{M1} \end{array}$ Rule. 4 Rule. 5

Increasing factor(S<sub>ci</sub>)

$$S_{ci1} = e^{(\frac{E_{M2}}{E_{M1}})^{1/2}}$$

Where

E<sub>M2</sub> 0.95x1/2 . F<sub>M1</sub> Rule.6

$$S_{ci2} = e^{(\frac{E_{M2}}{E_{M1}})^{1/2}} . e^{(\frac{F_1}{F_2} . \frac{V_2}{V_1})}$$

Where

$$E_{M2} > 1/2 .F_{M1}$$
 Rule . 7

So the general equation for case. 1 is:

$$n = \frac{F_1}{F_2} \frac{J/V}{\frac{V_2}{F_2} \frac{V_1}{F_1}} e^{-\left(\left|\frac{J_2}{V_2} \frac{J_1}{V_1}\right|\right)^{1/2} - (V_{M_1} - V_{M_2})^{1/2}} e^{-\left(\frac{E_{M_2}}{E_{M_1}}\right)^{1/2}} \dots Eq.2$$

n is subjected to correction factor under rules (4-7). e.g. Resorsinol/Water, Naphthalene/ Benzene, Benzoic acid /Methanol, Phenol/ Water, Resorsinol/ Methanol.

## Case. 2 : $V_1/F_1 - V_2/F_2 = J/V$

It taking the formula

$$n = \frac{F_1}{F_2} \cdot \left(\frac{V_2}{F_2} \cdot \frac{V_1}{F_1}\right) \cdot e^{-\left(\frac{J_2}{V_2} \cdot \frac{J_1}{V_1}\right)^{1/2}} \cdot e^{-\left(V_M_1 - V_{M_2}\right)^{1/2}} \cdot e^{-\left(\frac{E_{M_1}}{E_{M_2}}\right)^{1/2}} \cdot e^{-\left(\frac{E_{M_1}}{E_{M_2}}\right)^{1/2}} \cdot e^{-\left(\frac{E_{M_1}}{E_{M_2}}\right)^{1/2}}$$
Where the factor  $e^{-\left(\frac{E_{M_1}}{E_{M_2}}\right)^{1/2}}$  is applied when :

Rule. 8  $4.F_{M2}$   $E_{M1}$ n is subjected to decreasing factor under Rule.4,5 and increasing factor under Rule. 6 Increasing factor S<sub>ci3</sub>:

$$S_{ci3} = e^{(\frac{E_{M2}}{E_{M1}})^{1/2}} e^{(\frac{VM_2}{VM_1})}$$

The second part is applied only if  $V_{M2} < V_{M1}$  Rule. 9 e.g Benzoic acid /Water, Benzoic acid/ Dimethyl ether, Stearic acid / methanol **Case. 3:**  $V_1/F_1 - V_2/F_2 < J/V$ 

Eq.3, rule. 8 are applied here and n is subjected to decreasing  $(S_{cd})$  and increasing factors  $(S_{ci1}, S_{ci2})$  under rules 4-7.

Category 2: V<sub>1</sub>/F<sub>1</sub> V<sub>2</sub>/F<sub>2</sub> (V<sub>1</sub>/F<sub>1</sub> 0.95 V<sub>2</sub>/F<sub>2</sub>)

The solubility here depend on the interaction between energy per unit mass of solute and solvent  $(E_M)$ : It taking the formula:

$$n = \frac{F_1}{F_2} \cdot \frac{J_1/V_1}{J_2/V_2} \cdot e^{-(V_{M1} - V_{M2})} \cdot e^{(E_{M2}/E_{M1})} \dots \cdot Eq.4$$

e.g Salicylic acid / Methanol

**Category 3:**  $V_1/F_1 < V_2/F_2$ 

This category is divided into two cases:

Case. 4:  $V_1/F_1 - V_2/F_2 > J/V$ 

It is treated under Eq.2

e.g Succinic acid / Methanol, Oxalic acid / Methanol

### Case. 5: V1/F1 – V2/F2 J/V

It is treated under Eq.3

$$\mathbf{n} = \frac{F_1}{F_2} \cdot \left(\frac{V_2}{F_2} - \frac{V_1}{F_1}\right) e^{-\left(\frac{J_2}{V_2} - \frac{J_1}{V_1}\right)^{1/2}} \dots Eq.5$$

e.g Succinic acid /Water, Oxalic acid / Water, Salicylic acid / Chloroform

#### **Decreasing factor**

$$S_{cd2} = e^{-(E_{M2}/2.E_{M1})^{1/2}}$$

 $E_{M1} < 1/4$ .  $F_{M2}$ 

Rule. 10

$$S_{cd3} = e^{-(E_{M1}/2.E_{M2})1/2}$$

 $E_{M2} < 1/4. F_{M1}$ 

Rule. 11

**Increasing factor** 

$$e^{\left(\frac{E_{M-2}}{E_{M-1}}\right)^{1/2}}$$

Where

 $\begin{array}{ll} E_{M2} > E_{M1} , E_{M1} > 1/2 \ F_{M2} & \text{Rule. 12} \\ E_{M1} > E_{M2} , E_{M2} > 1/2 \ F_{M1} & \text{Rule. 13} \\ \end{array}$ 

Category 4: Solubility of solute with  $E_{\rm M2}$  < 1 in solvent with  $E_{\rm M1}$  > 1

It is\_treated under the categories above (mainly Eq.1) with the following correction factors:

#### **Decreasing factor**

$$S_{cd 4} = e^{-(5 - (\frac{E_M 2}{E_M 1}))} . e^{-(\frac{E_M 1}{E_M 2})^{1/2}}$$

Where 5.  $E_{M2} < 1/2 F_{M1}$  Rule. 14 e.g naphthalene/ water

**Increasing factor** 

$$S_{ci 4} = e^{(\frac{5 \cdot E_{M-2}}{E_{M-1}})}$$

# Category 5: Solubility of solute with $E_{\rm M2}$ > 1 in solvent with $E_{\rm MI}{<}$ 1

It is\_treated under the categories above (mainly Eq.1)

The factor 
$$e^{-(\frac{EM-2}{EM-1})^{1/2}}$$

Which is used under rule.3 is transformed to

$$e^{-(\frac{EM-2}{5\cdot EM-1})^{1/2}}$$

Where Rule. 16 e.g. Salicylic acid /Benzene

**Increasing factor** 

$$S_{ci5} = \frac{E_{M2}}{5.E_{M1}} \cdot \frac{V_2}{V_1}$$

Where Rule. 17 e.g.Benzoic/Benzene, Stearic/ Benzene, phenol/ Benzene

#### Effect of temperature

Here the temperature factor  $(T_f)$  is multiplied by all factors in the solubility equation or raised to a power equals to the number of factors in the equation. The increasing factor is not multiplied by  $T_f$ .

$$T_f = \left(\frac{T_s}{298}\right)^2$$

Where  $T_s$  is the absolute temperature e.g. Resorcinol/Water at 80°C(353 K), Benzoic acid / Boiling Methanol

additional T<sub>f</sub> factor is multiplied to become

$$\left(\frac{V}{F}\frac{2}{2}-\frac{V}{F}\frac{1}{1}\right)$$
.  $T_{f}^{2}$ 

If n is not subjected to a decreasing factor additional  $T_{\rm f}$  factor is multiplied also.

e.g Salicylic acid / Boiling Water, Benzoic acid/ Water at 95  $^{\circ}\mathrm{C}.$ 

#### A.2. Solubility of ionic solids

It involves two categories:

#### **Category 1:**

The factor  $F_{Latt}$  has to be compared with  $S_{gr}S_{ge}$ 

$$\frac{F_1.F_2}{(Latt.)^2} \geq S_{gr}.S_{ge}$$

The factor Sv has to be evaluated also ,  $2.E_{M2}>F_{M1}\,,~~a$  factor  $S_v$  has to be evaluated:

$$Sv = e^{-(\frac{E_{M2}}{F_{M1}})^{1/2}} \cdot \frac{V_2/F_2}{V_1/F_1}$$

Case  $1 S_v > 1$ 

$$\mathbf{n} = \frac{\mathbf{F}_1}{\mathbf{F}_2} \cdot S_{gr} \cdot S_{ge} \cdot S_{ci5} \cdot \dots \cdot Eq.6$$

 $S_{ci5}\xspace$  is considered  $F_{Latt}/n < 90$  %

$$S_{ci6} = \frac{F_{Latt}}{S_{gr} \cdot S_{ge}}$$

e.g .NaCl/water, NaBr/ water,NaNO3/water If  $S_{ci6} > F_{M1}$ 

Rule. 18 e.g KNO3/water

Case 2 :  $S_v < 1$ 

$$n = \frac{F_1}{F_2} \cdot e^{-(\frac{2.E_M 2}{V_2} - \frac{V_1}{F_2})^{1/2}} \dots Eq.7$$

it has to be multiplied by  $E_{M2}/F_{M1}$ 

e.g. KNO3/methanol NaNO3/methanol belong to category 2

$$-\left(\frac{E_{M2}}{E_{M1}}\right)^{1/2}$$

The factor  $\boldsymbol{\ell}$  In case 2 and at into the equation 6 If  $E_{M1} < 0.95 E_{M2}$ 

$$\mathbf{n} = \frac{F_1}{F_2} . S_{gr} . S_{ge} . e^{-\left(\frac{E_{M_2}}{E_{M_1}}\right)^{1/2}} ..... Eq. 8$$

NaCl/methanol

#### **Effect of Temperature**

1) If 2.  $E_{M2} < E_{M1}$ a factor  $T_{f2}$  is multiplied by  $n_{298}$  (solubility at 298 K)

$$T_{f2} = (S_{ci6})^{1/2} \cdot \frac{T_s}{298}$$

e.g. NaCl/water, NaBr/water, NaNO3/water, KNO3/water 2)If  $2.E_{M2} > E_{M1}$  a factor  $T_{f3}$  is multiplied by  $n_{298}$  (solubility at 298 K)

$$T_{f3} = (\frac{E_{M2}}{F_{Latt} / S_{gr} \cdot S_{ge}})^{1/2} \cdot \frac{298}{T_s}$$

e.g. NaBr/methanol

If 
$$E_{M2} < F_M$$

Category 2:

Where 
$$\frac{F_1 \cdot F_2}{(Latt.)^2} \langle S_{gr} \cdot S_{ge} \rangle$$

The following formula is applied

$$n = \frac{F_1}{F_2} \cdot \frac{F_1 \cdot F_2}{(Latt.)^2} \cdot e^{-\left[\frac{(Latt.)^2 + (F_2)^2}{F_1 \cdot (Latt.)}\right] n_i / q} \cdot \frac{V_{M2}}{V_{M1}} \dots Eq.9$$

Where (q equals to the absolute sum of charges)  $n_i$  is the total number of ions

The factor 
$$\frac{V_{M-2}}{V_{M-1}}$$
 is applied where  $q > n_i$ 

e.g LiF, CaF<sub>2</sub>, HgBr<sub>2</sub>, UO<sub>2</sub> in water

#### **B.** Miscibility

The solvents are to be miscible if they satisfy one of the conditions below:

1. 
$$V_{1}/F_{1} \quad V_{2}/F_{2} \quad (\frac{V_{1}}{F_{1}} / \frac{V_{2}}{F_{2}} \ge 0.95)$$
  
2.  $E_{M1} \quad 1/2.E_{M2}$ 

3. The factor  $(m_1)$  is 1

$$m_1 = \frac{J_2/V_2}{J_1/V_1} \cdot e^{-(\frac{E_{M2}}{E_{M1}})^{1/2}}$$

The subscript 1,2 refer to lower and high values of the entioned factors respectively. In the case where one solvent is of  $E_{M1} < 1$ , the solvents become miscible if they satisfy one of the following:

1. 
$$V_{1/F_{1}} V_{2/F_{2}} (\frac{V_{1}}{F_{1}} / \frac{V_{2}}{F_{2}} \ge 0.95$$
)  
2.  $E_{M1} 1/2.E_{M2}$ 

3. The factor  $(m_2)$  is 1

$$m_2 = \frac{J1/V1}{J2/V_2} \cdot e^{-(\frac{E_{M2}}{5.EM1})^{1/2}}$$

# Quantitation of the amount miscible in the immiscible solvents

The number of miscible moles of immiscible solvents with water can be obtained using the following formula:

$$n = \frac{V_w}{V_s} e^{-(\frac{J_2/F_2}{J_1/F_1})} \cdot e^{-(\frac{E_M 2}{E_M 1})} \cdot \dots \cdot Eq.10$$

Where

The subscripts w, s refer to water and the other immiscible solvent. The subscripts1,2 refer to lower and higher values of the mentioned factors

(either for water or the other solvent).

Where  $E_{M1} < 1$ :

$$n = \frac{V_{W}}{V_{1}} \cdot e^{-\left(\frac{J_{1}/F_{1}}{J_{W}/F_{W}}\right)^{1/2}} \cdot e^{-\left(\frac{E_{MW}}{5 \cdot E_{M1}} \cdot (5 - (\frac{E_{M1}}{E_{MW}}))^{1/2}} \dots \cdot Eq.11$$

Where the subscripts w,1 refer to water and the other immiscible solvent.

# **RESULTS AND DISCUSSION**

The potential energy of molecule is taking as its energy of formation as considered by the semi-empirical method of

calculation<sup>8</sup>. The interpotential between molecules is related to the energy of vaporization. As shown in Figure 1

#### The resultant force Is:

Repulsive from 0 to M. attractive from M to B but increasing with distance, and attractive from B to infinity but decreasing with distance. There is a position where the two forces balance, shown by M on the graph. This is the equilibrium position for molecules in the solid. For a molecule to be completely separated from its neighbour it must gain an amount of energy, represented by CM on the diagram which is the latent heat of vaporization  $^{10}$ . The enthalpies of formation, vaporization, fusion and lattice  $^{11-14}$  are subtracted from the value RT which R is gas constant and T is the absolute temperature (set at 298 K) to obtain the corresponding energies Tables (1-3). The solubility is a ratio between quantity of solute dissolved in a certain quantity of solvent so, we are studying the interaction between the ratios of energies of both solute and solvent; V/F, J/V and the ratios of the energies and the molar masses;  $F_M$ ,  $V_M$ E<sub>M</sub> Table 4. The results are compared with reported practical solubility <sup>15-17</sup>.



Figure 1 shows how the potential energy of two molecules

Table 1 The e	nthalpy of form	nation, vapo	prization,	fusion
	and la	ttice		

H Lattice	H <sub>fus</sub>	$H_{Vap}$	$\mathbf{H}_{\mathbf{f}}$	Name	
Ionic Compounds					
1036	27.09	322	616	LiF	
2630	30	441.4	1225.9	$CaF_2$	
2628	71.172	83.998	169.452	$HgBr_2$	
10644	70	619.3	1085	$UO_2$	
786	28.16	229	411.2	NaCl	
747	26.11	218	361.1	NaBr	
685.3	10.1	79.87	494.6	KNO3	
756	15	97.4	467.9	NaNO3	
	Ν	Ion ionic Com	pounds		
	32.4	117.5	940.5	Succinic acid	
	25	98.1	829.9	Oxalic	
	20.4	93.3	368	Resorcinol	
	18.02	91.2	385.2	Benzoic acid	
	11.51	68.7	165.1	Phenol	
	14.2	95	589.9	Salicylic	
	63	166.5	947.7	Stearic acid	
	19.01	72.1	78.5	Naphthalene	
		Solvents	3	•	
	6.01	44.016	285	Water	
	3.215	38.2	239.2	Methanol	
	5.37	47.5	302.6	Propanol	
	10.5	57	351.6	Pentanol	
	23.7	70.9	426.5	Octanol	
	9.87	33.83	49.1	Benzene	
	4.94	19.2	203.3	ether	
	10.48	35.6	479.3	Ethylacetate	
	9.5	31.4	134.1	Chloroform	

#### A. Solubility of solid in liquid

The solubility of solid materials in liquid is divided into solubility of non ionic solids and solubility of ionic solids.

solubility increases and vice versa. Different solutes and solvents with different energies were investigated to determine the concentration of the saturated solution or by other mean the solubility.

|--|

Latt.	J	V	F	Name
		Ionic Compoun	ds	
1033.522428	24.612428	319.522428	613.5224	LiF
2627.522428	27.522428	438.922428	1223.422	CaF2
2625.522428	68.694428	81.520428	166.9744	HgBr2
10641.52243	67.522428	616.822428	1082.522	UO2
783.522428	25.682428	226.522428	408.7224	NaCl
744.522428	23.632428	215.522428	358.6224	NaBr
753.522428	7.622428	77.392428	492.1224	KNO3
683.522428	12.522428	94.922428	465.4224	NaNO3
	N	on ionic Compo	unds	
	29.922428	115.022428	938.0224	Succinic acid
	22.522428	95.622428	827.4224	Oxalic acid
	17.922428	90.822428	365.5224	Resorcinol
	15.542428	88.722428	382.7224	Benzoic acid
	9.032428	66.222428	162.6224	Phenol
	11.722428	92.522428	587.4224	Salicylic acid
	60.522428	164.022428	945.2224	Stearic acid
	16.532428	69.622428	76.02243	Naphthalene
		Solvens		
	3.532428	41.538428	282.5224	Water
	0.737428	35.722428	236.7224	Methanol
	2.892428	45.022428	300.1224	Propanol
	8.022428	54.522428	349.1224	Pentanol
	21.222428	68.422428	424.0224	Octanol
	7.392428	31.352428	46.62243	Benzene
	2.462428	16.722428	200.8224	ether
	8.002428	33.122428	476.8224	Ethylacetate
	7.022428	28.922428	131.6224	Chloroform

 Table 3 The energy / mass ratios of the studied compounds

 Table 4 The ratios of different energies of the studied compounds

<b>F</b>	V.	F	Namo		······		
LM	V M Ionia Co	T M	Name	J/F	J/V	V/F	Name
20 81047104	6 150074065	22 65150707	LEE		Ionic Con	pounds	
29.0104/194	0.1300/4003	25.05159/07			0.077028796	0.520799914	LiF
16.49650625	2.813003308	13.06490292			0.062704538	0.358766047	CaF2
0.576384235	0.113094015	0.463290219	HgBr2		0.842665203	0.488221035	HgBr2
5.151090972	1.142149541	4.008941432	002		0.109468179	0.569801061	ŪO2
8.699/2/36/	1.88/6869	6.812040467	NaCl		0.113376977	0.554220695	NaCl
4.532837419	1.04/343901	3.485493517	NaBr		0.109651827	0.600973088	NaBr
5.2504316/2	0.382/51869	4.86/6/9802	KNO3		0.098490617	0.15726255	KNO3
6.0339252	0.558367224	5.475557976	NaNO3		0.131922753	0.203948977	NaNO3
	Non ionic	Compounds			Non ionic C	ompounds	
8.430295893	0.48701172	7.943284173	Succinic acid		0.260144291	0.122622258	Succinic acid
9.721577719	0.531058692	9.190519027	Oxalic acid		0.235534994	0.115566638	Oxalic
3.732028353	0.412416801	3.319611552	Resorcinol		0.197334826	0.248472928	Resorcinol
3.497245676	0.363259204	3.133986472	Benzoic acid		0.175180373	0.231819255	Benzoic acid
2.079838933	0.351835235	1.728003698	Phenol		0 136395301	0.407215836	Phenol
4.587920953	0.334934941	4.252986012	Salicylic acid		0.126698231	0 15750578	Salicylic
3.610916908	0.288284639	3.322632269	Stearic acid		0.368988734	0.173527863	Stearic acid
0.864739346	0.271601888	0.593137458	Naphthalene		0.237458366	0.915814317	Naphthalene
	Sol	vents			Solve	onte	raphinatene
16.84953567	1.153845222	15.69569044	Water	0.012503177	0.085040002	0 147027011	Water
7.950769582	0.557814304	7.392955278	Methanol	0.003115159	0.020643278	0.15090/282	Methanol
5.368280233	0.374562629	4.993717604	Propanol	0.009637494	0.064244158	0.15001354	Propanol
4.269808758	0.309259376	3.960549382	Pentanol	0.009037494	0.147130062	0.156160038	Pentanol
3.518648867	0.262698411	3.255950457	Octanol	0.022978839	0.14/139902	0.150109958	Octorol
0.797575752	0.200694072	0.59688168	Benzene	0.050050249	0.225784865	0.101303113	Panzana
4.540560929	0.181489342	4.359071587	ether	0.12261719	0.233764603	0.07247323	othor
5.600268354	0.187981998	5.412286356	Ethylacetate	0.012201/18	0.14/255019	0.063209/23	Ethvilagetete
1.223686061	0.121135986	1.102550075	Chloroform	0.010/82820	0.241001491	0.009404912	Chloroform
G 1 1 994		• •		0.055552822	0.24260210	0.219/3/84	Chiorotorm
. Solubility (	of non ionic soli	las		Category 1 · V.	$(\mathbf{F}_1 > \mathbf{V}_2 / \mathbf{F}_2)$		

The solubility of non ionic solutes was found to be affected mainly by the interaction between energy per unit mass of both solute and solvent. As  $E_{M1}$  is higher and close to  $E_{M2}$ , the

Category. 1 :  $V_1/F_1 > V_2/F_2$ Case 1:  $V_1/F_1 - V_2/F_2 > J/V$ 

The solubility was expressed in mole/mole. There are some systems (Solute/Solvent) fall in this category. Table 5.

e.g. Resorsinol/Water, Naphthalene/ Benzene, be Benzoic/Methanol, Phenol/ Water, Resorsinol/ Methanol. be

benzene where  $E_{M2}$  of naphthalene is higher than 0.95.  $E_{M1}$  of benzene.

Table 5	Calculated	and report	d value of	f solubilit	y of non	ionic con	pounds in	different solvent	ts

Solute/solvent	Calculated value of solubility	Reported value of solubility	Category
Resorcinol/Water	0.19	0.18	Category1, Case1
Resorcinol/ Methanol	0.453	0.4	Category1, Case1
Phenol/Water	0.0133	0.013	Category1, Case1
Benzoic acid/ Methanol	0.136	0.146	Category1, Case1
Naphthalene/Benzene	0.202	0.2	Category1, Case1
Benzoic acid/ Water	5.7x10 <sup>-4</sup>	5x10 <sup>-4</sup>	Category1, Case 2
Benzoic acid/ Dimethyl ether	0.16	0.17	Category1, Case 2
Stearic acid/Methanol	0.0072	0.007	Category1, Case 2
Salicylic acid /Water	$1.9 \times 10^{-4}$	$2.7 \times 10^{-4}$	Category1, Case 3
Salicylic acid / Dimethyl ether	0.188	0.15	Category1, Case 3
Salicylic acid / Methanol	0.09	0.1	Category 2
Succinic acid/Methanol	0.087	0.055	Category 3, Case 4
Oxalic/Methanol	0.27	0.18	Category 3, Case 4
Succinic acid/Water	0.0125	0.0117	Category 3, Case 5
Oxalic/ Water	0.036	0.028	Category 3, Case 5
Salicylic acid / Chloroform	0.01	0.013	Category 3, Case 5
Naphthalene/ Water	2.6x10-6	3.6x10-6	Category 4
Naphthalene/Methanol	0.019	0.015	Category 4
Salicylic/Benzene	0.0048	0.00532	Category 5
Benzoic/Benzene	0.074	0.07	Category 5
Stearic/ Benzene	0.075	0.07	Category 5
Phenol/ Benzene	0.1	0.08	Category 5

 Table 6 Calculated and reported value of solubility of ionic compounds in different solvents

Solute/solvent	Calculated value of solubility	Reported value of solubility	Category
NaCl/Water	0.12	0.11	Category1,Sv>1
NaBr/Water	0.146	0.15	Category 1,Sv>1
NaNO <sub>3</sub> /Water	0.17	0.19	Category 1,Sv>1
KNO <sub>3</sub> /Water	0.056	0.06	Category 1,Sv>1
NaCl/ Methanol	0.0077	0.007	Category 1,Sv>1
NaBr/ Methanol	0.1	0.066	Category 1,Sv>1
KNO <sub>3</sub> /Methanol	1.01x10 <sup>-7</sup>	insoluble	Category 1,Sv<1
NaNO <sub>3</sub> /Methanol	0.0026	0.0016	Category 2
LiF/Water	5.3x10 <sup>-4</sup>	$7.4 \times 10^{-4}$	Category 2
CaF <sub>2</sub> /Water	5.07 x10 <sup>-6</sup>	$4.5 \times 10^{-6}$	Category 2
HgBr2/Water	6.13x10 <sup>-7</sup>	4.02x10 <sup>-7</sup>	Category 2
UO2/Water	$3.37 \times 10^{-14}$	3.38x10 <sup>-14</sup>	Category 2

 Table 7 Calculated and reported value of the amount dissolved of different solvents in water

Solvent A/solvent B	Calculated value of solubility	Reported value of solubility
Ether/Water	0.0245	0.0277
Ethyl acetate/Water	0.018	0.017
Pentanol/Water	2.34x10 <sup>-3</sup>	4.5x10 <sup>-3</sup>
Octanol/Water	8.95x10 <sup>-5</sup>	6.36x10 <sup>-5</sup>
Benzene/Water	$4.24 \times 10^{-4}$	$4.12 \times 10^{-4}$

The solubility of resorsinol in water was not subjected to any correction factor while, the solubility of resorsinol in methanol is subjected to increasing factor  $S_{ci2}$  because  $E_{M2}$  of resorcinol is higher than 1/2  $F_{M1}$  of methanol. The solubility of benzoic acid in methanol is subjected to  $S_{ci1}$  because  $E_{M2}$  of benzoic acid is approximately equal to ( ) 0.95.1/2  $F_{M1}$  of methanol. The number of Phenol moles dissolved in mole of water is corrected by the decreasing factor  $S_{cd1}$  because  $E_{M2}$  of phenol is  $-\left(\frac{E_{M2}}{E_{M1}}\right)^{1/2}$ 

lower than 0.95. 1/4  $F_{M1}$  of water. The factor  $e^{E_{M_1}}$  is considered in determination of solubility of naphthalene in

Case. 2 :  $V_1/F_1 - V_2/F_2 = J/V$ 

The solubility of Benzoic acid in water, Benzoic in dimethyl ether, Stearic acid in methanol are examples of this case. The system Benzoic acid / water is subjected to a deceasing factor  $S_{cd1}$  where Benzoic / Dimethyl ether, Stearic acid / Methanol are subjected to increasing  $S_{ci1}$ ,  $S_{ci3}$  factors. Table 5.

## Case. 3: $V_1/F_1 - V_2/F_2 < J/V$

Eq.3, rule. 8 are applied here and n is subjected to decreasing (S<sub>cd</sub>) and increasing factors (S<sub>ci1</sub>, S<sub>ci2</sub>) under rules 4-7.e.g. Solubility of salicylic acid in water and salicylic acid in dimethyl ether. Table 5.

## Category 2: V<sub>1</sub>/F<sub>1</sub> V<sub>2</sub>/F<sub>2</sub> (V<sub>1</sub>/F<sub>1</sub> 0.95 V<sub>2</sub>/F<sub>2</sub>)

The solubility here depend on the interaction between energy per unit mass of solute and solvent ( $E_M$ ). The solubility is corrected by the increasing factor  $S_{ci1}$ . Table 5 e.g Salicylic acid / Methanol

#### Category 3: $V_1/F_1 < V_2/F_2$ Case. 4: V1/F1 - V2/F2 > J/V

e.g Succinic acid / Methanol, Oxalic acid / Methanol The energy per unit mass  $E_{\rm M2}$  of both succinic and oxalic acid are higher than  $E_{\rm M1}$  of methanol. Also,  $E_{\rm M2}$  of both solutes are higher than half of  $E_{\rm M1}$  of solvent so, the increasing factor  $S_{\rm ci1}$ is applied here. Table 5

## Case. 5: V1/F1 – V2/F2 J/V

e.g Succinic/Water, Oxalic/ Water, Salicylic/ Chloroform The energy per unit mass  $E_{M2}$  of both succinic and oxalic acidS are lower than  $E_{M1}$  of water. Also,  $E_{M2}$  of both solutes are higher than half of  $E_{\rm M1}$  of solvent so, the increasing factor  $S_{\rm ci1}$  is applied here. Table 5

# Category 4: Solubility of solute with $E_{\rm M2}$ < 1 in solvent with $E_{\rm MI}{>}$ 1

Dealing with energy per unit mass  $E_M$  less than one makes a calculation error and not matched with the experimental results. Multiplying the  $E_M$  by a factor of five gave a close results with the reported data.

#### e.g: Naphthalene/ Water, Naphthalene/Methanol

Where the solubility of naphthalene in water is corrected by the application of decreasing factor under rule 15. But the concentration of saturated solution of naphthalene in methanol is subjected to the increasing factor under rule 16. Table 5.

# Category 5: Solubility of solute with $E_{\rm M2}$ > 1 in solvent with $E_{\rm M1}{<}$ 1

e.g. Salicylic/Benzene, Benzoic/Benzene, Stearic/ Benzene, Phenol/ Benzene

The solubility equation of salicylic acid in benzene contain the

 $e^{-\left(\frac{EM}{5\cdot EM}\frac{2}{1}\right)^{1/2}}$ 

factor under rule 17. Where the solubility of benzoic acid, stearic acid, phenol in benzene is treated by multiplying by the increasing factor  $S_{ci4}$ .

#### **Effect of temperature**

The temperature factor  $(T_f)$  is multiplied by all factors in the solubility equation of resorcinol in water at 80°C (353 K) and benzoic acid in boiling methanol

The solubility equation of resorcinol in water at 298 K is:

$$n - 0.773 x \frac{0.085040002}{(0.248472928-0.147027011)} x e^{-(0.197334826-0.085040002)^{1/2}} x e^{-(1.153845222-0.412416801)^{1/2}}$$

Here we have four factors in the equation, so, the temperature factor  $T_f$  is raised to the forth power. The solubility of resorcinol in water at 80°C(353 K) was calculated to be 0.778 versus the reported value 0.82<sup>15</sup>. Where that of benzoic acid in boiling methanol was 0.36 versus 0.22<sup>15</sup>. The solubility of salicylic acid in boiling water was calculated to be 0.00675 versus 0.008<sup>15</sup> which is the reported value. The temperature factor ( $T_f$ ) is raised to eighth power as the equation contain sex factors. The other two powers are put because there is no decreasing factor. Also,  $T_f$  is raised to the seventh power in case solubility of benzoic acid in water at 95 °C to give 0.011 versus 0.01<sup>15</sup>.

#### A.2. Solubility of ionic solids

The solubility equation here deals mainly with water as solvent. The solubility of ionic compounds in different solvents depends mainly on the difference between (V/F) of solute and solvents, as the difference increase, the solubility increases. Also, the lattice energy of the ionic compound, the higher the

lattice energy the lower the solubility. The solubility of NaCl, NaBr, NaNO3 in water belong to category 1, as they have  $F_{Latt}$ 

 $S_{gr}. S_{ge}$  and Sv > 1. Their solubility equations are subjected to the increasing factor  $S_{ci5}$  except NaCl in water because  $F_{Latt}/n$  more than 90 % . In case of KNO<sub>3</sub> in water the increasing factor is multiplied by  $E_{M2}/F_{M1}$ . The solubilities of these compound in methanol were also treated in the same way. The  $-(\frac{E_{M2}}{2})^{1/2}$ 

factor  $e^{-(\frac{-m}{E_{M_1}})^{1/2}}$  is put in the equation of solubility of sodium chloride in methanol because  $E_{Ml} < 0.95 E_{M2}$ . Table 6

#### **Effect of Temperature**

The temperature factor  $T_{f2}$  was applied for the determination of solubility of NaCl, NaBr, NaNO<sub>3</sub>, KNO<sub>3</sub> in boiling water as 2.  $E_{M2} < E_{M1}$ . The results were 0.15 for NaCl in water versus 0.12<sup>15</sup>, 0.2 for NaBr in water versus 0.18<sup>15</sup>, 0.53 for NaNO<sub>3</sub> in water versus 0.35<sup>15</sup> and 0.235 for KNO<sub>3</sub> in water versus 0.336<sup>15</sup>. The temperature factor  $T_{f3}$  was applied for the determination of solubility of NaBr in methanol as  $2.E_{M2} > E_{M1}$ . The result was 0.0886 versus 0.0612<sup>15</sup>. Solubility that belong to category 2 is characterized by  $\frac{F_1 \cdot F_2}{(Latt .)^2} < S_{gr} \cdot S_{ge}$  The solubility of sodium nitrate in methanol lies in this category and not in category 1 because  $\frac{F_1 \cdot F_2}{(Latt .)^2} < S_{gr} \cdot S_{gr}$ 

 $S_{gr}$ . $S_{ge}$ . The solubility of different ionic compounds with different solubility products <sup>(17)</sup> are studied in water. The solubility products are converted to mole/ mole. Table 6 shows the comparison between the calculated values of solubility and the reported ones. The factor  $V_{M2}/V_{M1}$  is applied in the solubility wquation of CaF<sub>2</sub>, HgBr<sub>2</sub>, and UO<sub>2</sub> in water where the total charges are higher than the total number of ions. Uranium oxide is dissolved in water to produces five ions and eight total charges <sup>(17)</sup> so the ni/q equals 5/8.

$$UO_2 \Leftrightarrow U^{+4} + 4OH^{-1}$$

#### **B.** Miscibility

The miscibility of liquids depend the ratio (V/F) and the energy per unit mass  $E_M$ . The solvents are to be miscible if they satisfy one of the conditions below:

1. 
$$V_{1/F_{1}} V_{2/F_{2}} (\frac{V_{1}}{F_{1}} / \frac{V_{2}}{F_{2}} \ge 0.95$$

1

2. 
$$E_{M1}$$
 1/2. $E_{M2}$ 

3. The factor 
$$(m_1)$$
 is

$$m_1 = \frac{J_2/V_2}{J_1/V_1} \cdot e^{-(\frac{E_M 2}{E_M 1})^{1/2}}$$

The subscript 1, 2 refer to lower and high values of the mentioned factors respectively.

2

In the case where one solvent is of  $E_{M1} < 1$ , the solvents become miscible if they satisfy one of the following:

1. 
$$V_{1/F_{1}}$$
  $V_{2/F_{2}}$   $(\frac{V_{1}}{F_{1}} / \frac{V_{2}}{F_{2}} \ge 0.95)$ 

- 2.  $E_{M1} = 1/2.E_{M2}$
- 3. The factor  $(m_2)$  is 1

$$m_2 = \frac{J1/V1}{J2/V_2} \cdot e^{-(\frac{E_{M2}}{5.EM1})^{1/2}}$$

# Quantitation of the amount miscible in the immiscible solvents

The number of miscible moles of immiscible solvents with water are studied and found to be close to the reported values <sup>15, 16</sup>. Table 7.

# CONCLUSION

The provided methodology in determining the concentration of saturated solution of a solute in a certain solvent resemble a scheme. The steps of this scheme have to be followed in order to reach to the solubility equation of the solute in the solvent of study. The solubility can be predicted without the need of complicated computer programs. The miscibility of solvents is easily to be predicted and the amount that will dissolve in an immiscible solvent can also be quantified.

# References

- 1. Atikins, P.; De Paula, J. *Elements on Physical Chemistry*. 9<sup>th</sup>, Oxford University Press, 2010
- 2. Bouillot, B.; Teychené, S.; Biscans, B. An Evaluation of thermodynamic models for the prediction of drug and drug-like molecule solubility in organic solvents. *Fluid Phase Equilibria*, 2011, 309, 36-52
- 3. Bruno, J.; Bosbach, D.; Kulik, D.; Navrotsky, A.

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- 4. Budavari, S. *The Merk Index.* 14 <sup>th</sup> Ed, Merk and Co. Inc., White house station, NJ,USA, 2006
- Harris, D. *Exploring Chemical Analysis*. 5 <sup>TH</sup> Ed, W. H. Freeman and Company, New York, 2013
- Hojjati, H.; Rohani, S. Measurement and prediction of solubility of paracetamol in water – isopropanol solution. Part 2 prediction. Org. Process Res. DEV. 2006, 10, 1110-1118
- Hsieh, C.; Wang, S.; Lin, S.; Sandler, S. A Predictive model for the solubility and octanol-water partition coefficient of pharmaceuticals. *J. Chem. Eng.* 2011, 56, 936–945.
- 8. http:// enwikipedia.org
- 9. http:// webelements.com Accessed in 2014
- http://cool.conservationus.org/coolaic/sg/bpg/annual/v03/bp03-04.html. Accessed in 2014
- 11. http://home.engineering.iastate.edu "Hansen solubility parameters" Accessed in 2014
- 12. http://hyperphysics.phyastr.gsu.edu/hbase/hframe.html
- 13. http://nist.gov Accessed in 2014
- 14. http://schoolphysics.co.uk Accessed in 2014
- 15. http://update.uu.se/~jolkkonen/pdf/CRC\_TD.pdf Accessed in 2014
- 16. Lewars, E. Computational Chemistry. New York, 2006
- Rodgers, G. Descriptive Inorganic, Coordination, and Solid State Chemistry. 3<sup>rd</sup>, Allegheny College.USA, 2012

Wael Talaat., Thermodynamic Contribution to the Solubility Equation. International Journal of Recent Scientific Research Vol. 6, Issue, 4, pp.3461-3470, April, 2015

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